

UNITED STATES PATENT APPLICATION

TITLE: PROCESS AND APPARATUS FOR BOILING AND VAPORIZING MULTI-COMPONENT FLUIDS

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BACKGROUND OF THE INVENTION**1. Field of the Invention**

[0001] The present invention relates to an improved boiler apparatus, systems incorporating the boiler apparatus and to methods for making and using the boiler apparatus and systems incorporating the boiler apparatus.

[0002] More particularly, the present invention relates to an improved boiler apparatus, systems incorporating the boiler apparatus and to methods for making and using the boiler apparatus and systems incorporating the boiler apparatus, where the boiler apparatus includes a vapor removal unit that remove vapor as it boils so that the boiling throughout boiler's length remains substantially nucleate boiling.

2. Description of the Related Art

[0003] In several processes and especially in power systems using multi-component working fluids, it is necessary to completely vaporize such multi-component fluids. However, it is, in practice difficult to completely vaporize such multi-component fluid.

[0004] When a working fluid in the form of a saturated liquid is sent into a boiler, and the quantity of vapor in the stream of working fluid is relatively small, the boiling process is characterized as nucleate boiling. Nucleate boiling has a very high film heat transfer coefficient, but as vapor accumulates, a so-called crisis of boiling occurs. This crisis of boiling results in a drastic fall or reduction in the film heat transfer coefficient.

[0005] On the other hand, when a single-component fluid is vaporized, the liquid can be recycled within the heat exchanger and nucleate boiling can be sustained throughout the entire process. But, such an approach cannot be used with multi-component fluids, because the vapor produced will have a different composition (enriched by the low boiling component) than the remaining liquid resulting in a continuous composition profile across the heat exchanger with the concurrent crises of boiling.

[0006] Thus, if a multi-component fluid needs to be vaporized fully, the in a significant proportion of this vaporization process, *i.e.*, inside the heat exchanger or boiler, nucleate boiling cannot be maintained. Thus, the film heat transfer coefficient in such a process is very low. This results in

a very large increase in the required surface of the heat exchanger or boiler.

[0007] If complete vaporization of a multi-component working fluid has to be performed at high temperature, *e.g.*, in a furnace of a power plant, then the inability of the process to maintain nucleate boiling inside heat transfer tubes of the furnace makes such a process technically very difficult.

[0008] When nucleate boiling is maintained, due to a high film heat transfer coefficient, the temperature of the metal of the heat transfer tubes is maintained close to the temperature of the boiling fluid, and as a result the tubes are protected from burn out. However, because in the process of direct vaporization of multi-component working fluids where nucleate boiling cannot be maintained, the heat transfer tubes can achieve unacceptably high temperatures resulting in tube damage or destruction.

[0009] Thus, there is a need in the art for process and apparatus for boiling and vaporization of multi-component fluids designed to achieve the production of vapor of the same composition as the composition of the initial multi-component liquid, and at the same time, to maintain a process of nucleate boiling in the heat transfer apparatus.

SUMMARY OF THE INVENTION

[0010] The present invention provides an improved boiler apparatus including a heat transfer unit and a vapor removal/equilibration apparatus, where the heat transfer unit and the vapor removal/equilibration unit are configured in such a way as to support substantially nucleate boiling throughout the heat transfer unit and to ensure that the vapor produced is in substantial equilibrium with the whether the boiling apparatus is used to substantially fully or completely vaporize or to partially vaporize a multi-component working fluid, where the multi-component working fluid comprises at least one lower boiling component and at least one higher boiling component

[0011] The present invention also provides an improved vaporization apparatus for multi-component working fluids including a plurality of heat transfer apparatuses, each apparatus including a heat exchange unit and a vapor removal or collector unit, where the vapor collector units are adapted to maintain substantially nucleate boiling throughout each heat exchange unit and where the vaporization apparatus converts a portion of a liquid multi-component fluid feed stream having a given composition into a vapor stream having substantially the same composition.

[0012] The present invention provides a system for extracting heat from a heat source and converting a portion of the heat into a useable form of energy including a heat source stream, a multi-component working fluid, a vaporization apparatus of this invention, and a heat extraction system.

[0013] The present invention provides a method for vaporizing a liquid multi-component working fluid having a given composition into a vapor multi-component working fluid having substantially the same compositions, where the method includes the step of feeding a liquid stream of the multi-component working fluid into an improved multi-component working fluid vaporization apparatus of this invention, where the stream can be from a energy production facility. The stream is heated by a heat source stream from a heat source, which leaves the apparatus as a spent heat source stream and sending a vapor multi-component working fluid stream back to the energy production facility, where the liquid multi-component working fluid and the vapor multi-component working fluid have substantially the same composition and the vaporization apparatus maintains substantially nucleate boiling throughout all heat exchange units.

[0014] The present invention provides a methods for vaporizing a multi-component working fluid having a given composition including the steps feeding an input stream comprising a multi-component working fluid having a given composition into one or a plurality of heat transfer apparatuses, each heat transfer apparatus including a heat exchange unit and a vapor equilibration unit and transferring heat from a heat source to a liquid portion of the input stream in such a way as to produce a vapor stream and optionally a remaining liquid stream, where the vapor stream and the remaining liquid stream have substantially the same compositions as the input stream. The vapor removal units associated with each heat transfer apparatus ensure that substantially nucleate boiling occurs throughout each heat exchange unit and ensure that the liquid and vapor are substantially equilibrated.

DESCRIPTION OF THE DRAWINGS

[0015] The invention can be better understood with reference to the following detailed description together with the appended illustrative drawings in which like elements are numbered the same:

[0016] **Figure 1** depicts a diagram of a preferred embodiment of a heat transfer apparatus of this invention having a vapor removal apparatus;

[0017] **Figure 2** depicts a diagram of another preferred embodiment of a heat transfer apparatus of this invention having a vapor removal apparatus;

[0018] **Figure 3** depicts a diagram of another preferred embodiment of a heat transfer apparatus of this invention having a vapor removal apparatus;

[0019] **Figure 4** depicts a diagram of another preferred embodiment of a heat transfer apparatus of this invention having a vapor removal apparatus;

[0020] **Figure 5** depicts a diagram of a preferred embodiment of a heat transfer apparatus of this

invention for use in high temperature furnace applications;and

[0021] **Figure 6** depicts a diagram of heat extraction and useable energy production facility including a multi-component vaporization apparatus of this invention.

DETAILED DESCRIPTION OF THE INVENTION

[0022] The inventors have found that a heat transfer apparatus can be constructed for substantially, fully vaporizing a working fluid comprising at least two components one component having a boiling point less than the other component or at least one lower boiling component and at least one higher boiling component, which includes a vapor removal system adapted to maintain substantially nucleate boiling in a boiling/vaporization zone of the apparatus.

[0023] The present invention broadly relates to an improved boiling apparatus for substantially completely vaporizing a multi-component fluid to obtain a desired vapor stream having a desired temperature and composition, where the boiling apparatus includes at least one heat transfer apparatus, where each heat transfer apparatus comprises a heat exchanger, heat transfer loop or mixture thereof and a vapor removal apparatus. The removal of vapor at each heat transfer stage maintains nucleate boiling in each of the heat transfer apparatuses. The heat transfer unit includes a liquid shell, a vapor shell and a plurality of connecting pipes which allow vapor and liquid to exchange between the liquid shell and the vapor shell. The plurality of connecting pipes is at least 2, the basic start for a plurality, preferably between about 2 and about 20, preferably, between about 4 and about 20 and particularly between about 5 and about 20. Moreover, the present invention can include an elongated slot with perforations for better exchange of vapor and liquid between the liquid shell and the vapor shell.

[0024] The present invention also broadly relates to a method for substantially maintaining nucleate boiling through each stage of a boiling apparatus including the steps of feeding a multi-component stream into at least one heat transfer apparatus, each heat transfer apparatus includes a vapor collectors or separator apparatus, where the apparatus allows substantially complete vaporization of the multi-component fluid while maintaining nucleate boiling throughout each heat transfer apparatus.

[0025] The working fluids to be vaporized in the inventions of this application are multi-component fluids that comprises a lower boiling point component fluid – the low-boiling component – and a higher boiling point component – the high-boiling component. Preferred working fluids include, without limitation, an ammonia-water mixture, a mixture of two or more hydrocarbons, a mixture of two or more freon, a mixture of hydrocarbons and freon, or the like. In general, the fluid can

comprise mixtures of any number of compounds with favorable thermodynamic characteristics and solubility. In a particularly preferred embodiment, the fluid comprises a mixture of water and ammonia.

[0026] It should be recognized by an ordinary artisan that at those point in the systems of this invention where a stream is split into two or more sub-streams, the valves that effect such stream splitting are well known in the art and can be manually adjustable or are dynamically adjustable so that the splitting achieves the desired improvement in efficiency. It should also be recognized that stream mixing is affected by an mixer valve also well known in the art.

[0027] Suitable heat exchange units include, without limitation, heat exchangers, heat transfer loops, or any other unit that can transfer heat from a heat source to a working fluid stream. Suitable vapor removal units include, without limitation, vapor/liquid separators such as drums or separation tanks, vapor collector or any other unit that can remove a vapor from a mixed vapor-liquid stream.

[0028] The term substantially when used with a composition means that the composition to two streams differs by no more than 5% in each component, preferably, no more than 2% in each component, particularly, no more than 1% in each component and especially, no more than 0.5% in each component, with zero (identical streams) being the ultimate goal. The term substantially when used in conjunction with nucleate boiling means that no more than 10% of the boiling that occurs in the heat exchange units is non-nucleate boiling, preferably, no more than 5% of the boiling that occurs in the heat exchange units is non-nucleate boiling, particularly, no more than 2.5% of the boiling that occurs in the heat exchange units is non-nucleate boiling, especially, no more than 1% of the boiling that occurs in the heat exchange units is non-nucleate boiling, with the ultimate goal being 0% of the boiling that occurs in the heat exchange units is non-nucleate boiling.

[0029] In several processes and especially in power systems using multi-component working fluids, it is necessary to completely vaporize such multi-component fluids. However it is, in practice, difficult to obtain complete vaporization directly for the following reasons.

[0030] When a working fluid in the form of saturated liquid is sent into a boiler, and the quantity of vapor in the stream of working fluid is relatively small, the boiling process is characterized as a nucleate boiling. Such a boiling process has a very high film heat transfer coefficient, but as vapor accumulates, a so-called crisis of boiling occurs, and the heat transfer coefficient drastically falls. Therefore, when single-component fluids are vaporized, the liquid is recycled within the heat exchanger and nucleate boiling can be sustained throughout the entire process. But, such an approach cannot be used directly when it is necessary to vaporize a multi-component fluid, because

the vapor produces will have a different composition (enriched by the low boiling component). Thus, if a multi-component fluid needs to be vaporized fully, in a significant proportion of the vaporization process, nucleate boiling cannot be maintained, and thus the heat transfer coefficient in such a process is very low. This results in a very large increase in the required surface area of the heat exchanger.

[0031] If complete vaporization of a multi-component working fluid has to be performed at high temperature, *e.g.*, in a furnace of a power plant, then the inability of the process to maintain nucleate boiling inside heat transfer tubes makes such a process technically very difficult. When nucleate boiling is maintained, due to a high film heat transfer coefficient, the temperature of the metal of the heat transfer tubes is maintained close to the temperature of the boiling fluid, and as a result the tubes are protected from burn out. However, because in the process of direct vaporization of multi-component working fluid, nucleate boiling cannot be maintained the heat transfer tubes will attain an unacceptably high temperature and will be destroyed.

[0032] The apparatus of this invention for boiling and vaporization of multi-component fluids is designed to achieve the production of vapor of the same composition as the composition of the initial multi-component liquid, (in case of complete vaporization) or vapor which is in equilibrium with liquid exiting the apparatus (in case of partial vaporization) and at the same time, to maintain a process of nucleate boiling in the heat transfer apparatus(es).

[0033] Unlike the systems disclosed in co-pending United States Application Serial No. 10/617367 filed 10 July 2003 and incorporated herein by reference, the systems of this invention are designed to operate effectively without a scrubber. The removal of the scrubber greatly simplifies the boiling equipment construction, system design, system cost and system simplicity.

[0034] Referring now to **Figure 1**, a flow diagram of a preferred embodiment of a boiling apparatus of this invention generally **100**, is shown to include a liquid shell **LSh**, which is in essence a standard horizontally disposed shell-and-tube heat exchanger, a vapor shell **VSh**, which comprises a horizontal drum or hollow vessel installed above the liquid shell **LSh**, and a plurality of vertically disposed, connecting pipes **CPs**, which interconnect the liquid shell **LSh** and the vapor shell **Vsh**. The liquid shell **LSh** also includes a liquid stream inlet **102** and a liquid stream outlet **104**. The liquid shell **LSh** further includes a heat source stream input **106**, a plurality of heat transfer tubes **108** and a heat source stream output **110**. The vapor shell **VSH** includes a vapor stream input **112** and a vapor stream output **114**.

[0035] The apparatus **100** is designed to operate with an entire volume of the liquid shell **LSh**, an

entire volume of the connecting tubes **CPs** and a lower portion of the vapor shell **VSh** being filled with liquid as shown by the dotted areas of the **LSh** and **VSh**. This configuration ensures that vaporization occurs in the liquid shell **LSh** in a substantially nucleate boiling process and that the produced vapor is sufficiently mixed with the liquid so that the liquid and vapor exiting the apparatus 100 are in equilibrium or are in substantial equilibrium.

[0036] The apparatus 100 of this invention operates by feeding a heat source stream 120, a hot liquid stream such as a geothermal brine stream, having initial parameters as at a point 3 into the liquid shell **LSh** via the heat source stream input 106. The heat source stream 120 passes through the heat transfer tubes 108 where it is cooled and leaves the liquid shell **LSh** as a spent heat source stream 122 having parameters as at a point 4 via the heat source stream output 110.

[0037] The apparatus 100 of **Figure 1** is designed to operate on a partially vaporize or mixed input stream (not shown) which is to be subjected to boiling and vaporization and further but not completely vaporized within the apparatus 100. In other words, the described process of **Figure 1** is a process of intermediate vaporization, as distinct from initial or final vaporization. The mixed stream enters the apparatus 100 as a liquid input stream 124 having parameters as at a point 1' via the liquid input 102 of the liquid shell **LSh**, while a vapor input stream 126 having parameters as at a point 1" via the vapor input 112 of the vapor shell **VSh**. The liquid input stream 124 passes through the liquid shell **LSh** where it is heated by the heat source stream and partially boils exiting the liquid shell **LSh** as a non-boiled liquid stream 128 having parameters as at a point 2' via the liquid output 104 of the liquid shell **LSh**. The vapor input stream 126 passes through the vapor shell **VSh** where it is fully mixed with the boiling liquid from the input liquid stream 124 rising up through the connecting tube **CPs** to form an output vapor stream 130 having parameters as at a point 2" via the vapor output 114 of the vapor shell **VSh**.

[0038] The stream to be further vaporized, which is comprised from a stream of vapor and a stream of liquid, enters into the apparatus as the liquid stream 124 and the vapor stream 126. The vapor stream 126 having the parameters as at the point 1" enters into the vapor shell **VSh** via the input 112 and the liquid stream 124 having the parameters as at the point 1' enters into the liquid shell **LSh** via the input 102. As a result of heating, the liquid of the stream 124 which fills the liquid shell **LSh**, the connecting pipes **CPs** and the lower portion of the vapor shell **VSh**, varies its temperature and composition along a length of the apparatus 100; the stream 124 is cool and rich in light-component composition at a cold end 132 of the apparatus 100, and the stream 124 is hot and lean in light-component composition at a hot end 134 of the apparatus 100. As the liquid boils throughout the

apparatus 100, bubbles of vapor move up and through the connecting pipes **Cps** and into the vapor shell **VSh**, carrying with them liquid (*i.e.*, creating a thermo-syphoning effect). As a result of this thermo-syphoning, a significant quantity of liquid is delivered to the vapor shell **VSh** where it is thoroughly mixed with vapor in the vapor stream 126, bringing the vapor in the stream 126 into equilibrium with the liquid in the stream 124. It is self-evident that each connecting pipe **CP** delivers liquid having a different temperature and composition into the vapor shell **VSh**. With each addition of boiling liquid into the vapor in the vapor shell **VSh**, the vapor in the vapor shell **VSh** is brought step-wise into equilibrium with the liquid in the liquid shell **LSh**. Of course, as boiling liquid in the liquid shell **LSh** is moving up through the connecting pipes **CPs** and into the vapor shell **VSh**, liquid in the **VSh** is continually flowing down into the liquid shell **LSh**, an integral part of the mixing and equilibration process. As a result, the heat from the heat source fluid is transferred to the boiling liquid in a process of nucleate boiling, and then transferred to the vapor by way of mixing (*i.e.*, direct contact heat and mass transfer).

[0039] Again, vapor produced in the apparatus 100 is then removed from the vapor shell **VSh** as the output vapor stream 130 having the parameters as at the point 2", while the remaining, non-vaporized liquid stream 128 is removed from the liquid shell **LSh** having the parameters as at the point 2'. Due to the intensive mixing of liquid and vapor achieved in the vapor shell **VSh** via the connecting pipes **CPs**, vapor and liquid of the stream 130 and 128 having the parameters as at the points 2" and 2', respectively, are in equilibrium or very close to equilibrium, which is the purpose of the apparatus 100.

[0040] Referring now to **Figure 2**, a flow diagram of a preferred embodiment of an initial boiling apparatus of this invention generally 200, is shown to include a liquid shell **LSh**, which is in essence a standard horizontally disposed shell-and-tube heat exchanger, a vapor shell **VSh**, which comprises a horizontal drum or hollow vessel installed above the liquid shell **LSh**, and a plurality of vertically disposed, connecting pipes **CPs**, which interconnect the liquid shell **LSh** and the vapor shell **Vsh**. The liquid shell **LSh** also includes a liquid stream inlet 202 and a liquid stream outlet 204. The liquid shell **LSh** further includes a heat source stream input 206, a plurality of heat transfer tubes 208 and a heat source stream output 210. In this embodiment, the vapor shell **VSH** include only a vapor stream output 214. In a case, the apparatus of this invention functions as an initial vaporization unit, *i.e.*, the stream to be vaporized is comprised only of saturated liquid, then vapor is not introduced into the vapor shell **VSh**.

[0041] Like the apparatus 100 of **Figure 1**, the apparatus 200 is designed to operate with an entire

volume of the liquid shell **LSh**, an entire volume of the connecting tubes **CPs** and a lower portion of the vapor shell **VSh** being filled with liquid as shown by the dotted areas of the **LSh**, **CPs** and **VSh**. This configuration ensures that vaporization occurs in the liquid shell **LSh** in a substantially nucleate boiling process and that the produced vapor is sufficiently mixed with the liquid so that the liquid and vapor exiting the apparatus **200** are in equilibrium or are in substantial equilibrium.

[0042] The apparatus **200** of this invention operates by feeding a heat source stream **220**, a hot liquid stream such as a geothermal brine stream, having initial parameters as at a point **23** into the liquid shell **LSh** via the heat source stream input **206**. The heat source stream **220** passes through the heat transfer tubes **208** where it is cooled and leaves the liquid shell **LSh** as a spent heat source stream **222** having parameters as at a point **24** via the heat source stream output **210**.

[0043] The apparatus **200** of **Figure 2** is designed to operate on a saturated liquid which is to be subjected to boiling and vaporization, but not complete vaporization. In other words, the described process of **Figure 2** is a process of initial partial vaporization, as distinct from intermediate or final vaporization. The liquid enters the apparatus **200** as a saturated liquid input stream **224** having parameters as at a point **21'** via the liquid input **202** of the liquid shell **LSh**. The liquid input stream **224** passes through the liquid shell **LSh** where it is heated by the heat source stream **220** and partially boils exiting the liquid shell **LSh** as a non-boiled liquid stream **228** having parameters as at a point **22'** via the liquid output **204** of the liquid shell **LSh**. As liquid of input stream **224** boils in the liquid shell **LSh**, the boiling liquid from the input liquid stream **224** rises up through the connecting tube **CPs** and into the vapor shell **VSh** where the produced vapor is fully mixed with the liquid to form an output vapor stream **230** having parameters as at a point **22''** via the vapor output **214** of the vapor shell **VSh**. As a result of heating, the liquid of the stream **224** which fills the liquid shell **LSh**, the connecting pipes **CPs** and the lower portion of the vapor shell **VSh**, varies in temperature and composition along a length of the apparatus **200**; the stream **224** is cool and rich in light-component composition at a cold end **232** of the apparatus **200**, and the stream **224** is hot and lean in light-component composition at a hot end **234** of the apparatus **200**. As the liquid boils throughout the apparatus **200**, bubbles of vapor move up and through the connecting pipes **Cps** and into the vapor shell **VSh**, carrying with them liquid (*i.e.*, creating a thermo-syphoning effect). As a result of this thermo-syphoning, a significant quantity of liquid is delivered into the vapor shell **VSh** where it is thoroughly mixed with the vapor in the vapor shell **VSh**, bringing the vapor into equilibrium with the liquid in the stream **124**. It is self-evident that each connecting pipe **CP** delivers liquid having a different temperature and composition into the vapor shell **VSh**. With each addition

of boiling liquid into the vapor shell **VSh**, the vapor in the vapor shell **VSh** is brought step-wise, step-by-step, into equilibrium with the liquid in the liquid shell **LSh**. Of course, as boiling liquid in the liquid shell **LSh** moves up through the connecting pipes **CPs** and into the vapor shell **VSh**, liquid in the **VSh** is continually flowing down into the liquid shell **LSh**, an integral part of the mixing and equilibration process. As a result, the heat from the heat source fluid is transferred to the boiling liquid in a process of nucleate boiling, and then transferred to the vapor by way of mixing (*i.e.*, direct contact heat and mass transfer).

[0044] Again, vapor produced in the apparatus 200 is then removed from the vapor shell **VSh** as the output vapor stream 230 having the parameters as at the point 22", while the remaining, non-vaporized liquid stream 228 is removed from the liquid shell **LSh** having the parameters as at the point 22'. Due to the intensive mixing of liquid and vapor achieved in the vapor shell **Vsh** via the connecting pipes **CPs**, vapor and liquid of the stream 230 and 228 having the parameters as at the points 22" and 22', respectively, are in equilibrium or very close to equilibrium, which is the purpose of the apparatus 200.

[0045] Referring now to **Figure 3**, a flow diagram of a preferred embodiment of a final boiling apparatus of this invention generally 300, is shown to include a liquid shell **LSh**, which is in essence a standard horizontally disposed shell-and-tube heat exchanger, a vapor shell **VSh**, which comprises a horizontal drum or hollow vessel installed above the liquid shell **LSh**, and a plurality of vertically disposed, connecting pipes **CPs**, which interconnect the liquid shell **LSh** and the vapor shell **Vsh**. The liquid shell **LSh** also includes only a liquid stream inlet 302. The liquid shell **LSh** further includes a heat source stream input 306, a plurality of heat transfer tubes 308 and a heat source stream output 310. The vapor shell **VSH** includes a vapor stream input 312 and a vapor stream output 314. In a case, the apparatus of this invention functions as a final vaporization apparatus, *i.e.*, all liquid introduced into the apparatus is vaporized.

[0046] Like the apparatuses 100 and 200 of **Figure 1** and **2**, the apparatus 300 is designed to operate with an entire volume of the liquid shell **LSh**, an entire volume of the connecting tubes **CPs** and a lower portion of the vapor shell **VSh** being filled with liquid as shown by the dotted areas of the **LSh** and **VSh**. This configuration ensures that vaporization occurs in the liquid shell **LSh** in a substantially nucleate boiling process and that the produced vapor is sufficiently mixed with the liquid so that the liquid and vapor exiting the apparatus 300 are in equilibrium or are in substantial equilibrium.

[0047] The apparatus 300 of this invention operates by feeding a heat source stream 320, a hot

liquid stream such as a geothermal brine stream, having initial parameters as at a point 33 into the liquid shell **LSh** via the heat source stream input 306. The heat source stream 320 passes through the heat transfer tubes 308 where it is cooled and leaves the liquid shell **LSh** as a spent heat source stream 322 having parameters as at a point 34 via the heat source stream output 310.

[0048] The apparatus 300 of **Figure 3** is designed to operate on a partially vaporize or mixed input stream (not shown) which is to be subjected to complete boiling and vaporization in the apparatus 300. In other words, the described process of **Figure 3** is a process of final vaporization, as distinct from initial or intermediate vaporization. The mixed stream enters the apparatus 300 as a liquid input stream 324 having parameters as at a point 31' via the liquid input 302 of the liquid shell **LSh**, while a vapor input stream 326 having parameters as at a point 31" enters the vapor shell **VSh** via the vapor input 312 of the vapor shell **VSh**. The liquid input stream 324 passes through the liquid shell **LSh** where it is heated by the heat source stream and completely boils. The vapor input stream 326 passes through the vapor shell **VSh** where it is fully mixed with the boiling liquid from the input liquid stream 324 rising up through the connecting tube **CPs** to form an output vapor stream 328 having parameters as at a point 2" via the vapor output 314 of the vapor shell **VSh**.

[0049] The stream to be further vaporized, which is comprised from a stream of vapor and a stream of liquid, enters into the apparatus as the liquid stream 324 and the vapor stream 326. The vapor stream 326 having the parameters as at the point 31" enters into the vapor shell **VSh** via the input 312 and the liquid stream 324 having the parameters as at the point 31' enters into the liquid shell **Lsh** via the input 302. As a result of heating, the liquid of the stream 324 which fills the liquid shell **LSh**, the connecting pipes **CPs** and the lower portion of the vapor shell **VSh**, varies its temperature and composition along a length of the apparatus 300; the stream 324 is cool and rich in light-component composition at a cold end 330 of the apparatus 300, and the stream 324 is hot and lean in light-component composition at a hot end 332 of the apparatus 300. As the liquid boils throughout the apparatus 300, bubbles of vapor move up and through the connecting pipes **Cps** and into the vapor shell **VSh**, carrying with them liquid (*i.e.*, creating a thermo-syphoning effect). As a result of this thermo-syphoning, a significant quantity of liquid is delivered to the vapor shell **VSh** where it is thoroughly mixed with vapor in the vapor stream 326, bringing the vapor in the stream 326 into equilibrium with the liquid in the stream 324. It is self-evident that each connecting pipe **CP** delivers liquid having a different temperature and composition into the vapor shell **VSh**. With each addition of boiling liquid into the vapor in the vapor shell **VSh**, the vapor in the vapor shell **VSh** is brought step-wise into equilibrium with the liquid in the liquid shell **LSh**. Of course, as boiling liquid in the

liquid shell **LSh** is moving up through the connecting pipes **CPs** and into the vapor shell **VSh**, liquid in the **VSh** is continually flowing down into the liquid shell **LSh**, an integral part of the mixing and equilibration process. As a result, the heat from the heat source fluid is transferred to the boiling liquid in a process of nucleate boiling, and then transferred to the vapor by way of mixing (*i.e.*, direct contact heat and mass transfer).

[0050] Again, vapor produced in the apparatus 300 is then removed from the vapor shell **VSh** as the output vapor stream 330 having the parameters as at the point 32", and because the apparatus is a final vaporization unit, no remaining, non-vaporized liquid is produced. Due to the intensive mixing of liquid and vapor achieved in the vapor shell **Vsh** via the connecting pipes **CPs**, vapor the stream 330 having the parameters as at the points 2" is in equilibrium or very close to equilibrium with the liquid in the liquid shell **LSh** having a composition that is that same as the overall composition of the input stream, which is the purpose of the apparatus 300.

[0051] It is also clear that if the whole process of vaporization, from a state of saturated liquid to a state of saturated vapor, occurs in only one apparatus, then the entire stream introduced into the apparatus is comprised only of saturated liquid as shown in **Figure 2**, and the entire stream removed from the apparatus is comprised only of saturated vapor as shown in **Figure 3**.

[0052] Referring now to **Figure 4**, a flow diagram of a preferred embodiment of a boiling apparatus of this invention, generally 400, is shown to include a liquid shell **LSh**, which is in essence a standard horizontally disposed shell-and-tube heat exchanger, a vapor shell **VSh**, which comprises a horizontal drum or hollow vessel installed above the liquid shell **LSh**, and a plurality of vertically disposed, connecting pipes **CPs**, which interconnect the liquid shell **LSh** and the vapor shell **Vsh**. The liquid shell **LSh** also includes a liquid stream inlet 402 and a liquid stream outlet 404. The liquid shell **LSh** further includes a heat source stream input 406, a plurality of heat transfer tubes 408 and a heat source stream output 410. The vapor shell **VSH** includes a vapor stream input 412 and a vapor stream output 414.

[0053] The apparatus 400 is designed to operate with an entire volume of the liquid shell **LSh**, an entire volume of the connecting tubes **CPs** and a lower portion of the vapor shell **VSh** being filled with liquid as shown by the dotted areas of the **LSh** and **VSh**. This configuration ensures that as vaporization occurs in the liquid shell **LSH** in a substantially nucleate boiling process, the produced vapor is sufficiently mixed with the liquid so that the liquid and vapor exiting the apparatus 400 are in equilibrium or are in substantial equilibrium.

[0054] The apparatus 400 of this invention operates by feeding a heat source stream 420, a hot

liquid stream such as a geothermal brine stream, having initial parameters as at a point 3 into the liquid shell **LSh** via the heat source stream input 406. The heat source stream 420 passes through the heat transfer tubes 408 where it is cooled and leaves the liquid shell **LSh** as a spent heat source stream 422 having parameters as at a point 4 via the heat source stream output 410.

[0055] The apparatus 400 of **Figure 4** is designed to operate on a partially vaporize or mixed input stream (not shown) which is to be subjected to boiling and vaporization and further but not completely vaporized within the apparatus 400. In other words, the described process of **Figure 4** is a process of intermediate vaporization, as distinct from initial or final vaporization. The mixed stream enters the apparatus 400 as a liquid input stream 424 having parameters as at a point 1' via the liquid input 402 of the liquid shell **LSh**, while a vapor input stream 426 having parameters as at a point 1'' via the vapor input 412 of the vapor shell **VSh**. The liquid input stream 424 passes through the liquid shell **LSh** where it is heated by the heat source stream and partially boils exiting the liquid shell **LSh** as a non-boiled liquid stream 428 having parameters as at a point 2' via the liquid output 404 of the liquid shell **LSh**. The vapor input stream 426 passes through the vapor shell **VSh** where it is fully mixed with the boiling liquid from the input liquid stream 424 rising up through the connecting tube **CPs** to form an output vapor stream 430 having parameters as at a point 2'' via the vapor output 414 of the vapor shell **VSh**.

[0056] The stream to be further vaporized, which is comprised from a stream of vapor and a stream of liquid, enters into the apparatus as the liquid stream 424 and the vapor stream 426. The vapor stream 426 having the parameters as at the point 1'' enters into the vapor shell **VSh** via the input 412 and the liquid stream 424 having the parameters as at the point 1' enters into the liquid shell **LSh** via the input 402. As a result of heating, the liquid of the stream 424 which fills the liquid shell **LSh**, the connecting pipes **CPs** and the lower portion of the vapor shell **VSh**, varies its temperature and composition along a length of the apparatus 400; the stream 424 is cool and rich in light-component composition at a cold end 432 of the apparatus 400, and the stream 424 is hot and lean in light-component composition at a hot end 434 of the apparatus 400. As the liquid boils throughout the apparatus 400, bubbles of vapor move up and through the connecting pipes **Cps** and into the vapor shell **VSh**, carrying with them liquid (*i.e.*, creating a thermo-syphoning effect). As a result of this thermo-syphoning, a significant quantity of liquid is delivered to the vapor shell **VSh** where it is thoroughly mixed with vapor in the vapor stream 426, bringing the vapor in the stream 426 into equilibrium with the liquid in the stream 424. It is self-evident that each connecting pipe **CP** delivers liquid having a different temperature and composition into the vapor shell **VSh**. With each addition

of boiling liquid into the vapor in the vapor shell **VSh**, the vapor in the vapor shell **VSh** is brought step-wise into equilibrium with the liquid in the liquid shell **LSh**. Of course, as boiling liquid in the liquid shell **LSh** is moving up through the connecting pipes **CPs** and into the vapor shell **VSh**, liquid in the **VSh** is continually flowing down into the liquid shell **LSh**, an integral part of the mixing and equilibration process. As a result, the heat from the heat source fluid is transferred to the boiling liquid in a process of nucleate boiling, and then transferred to the vapor by way of mixing (*i.e.*, direct contact heat and mass transfer).

[0057] Again, vapor produced in the apparatus 400 is then removed from the vapor shell **VSh** as the output vapor stream 430 having the parameters as at the point 2'', while the remaining, non-vaporized liquid stream 428 is removed from the liquid shell **LSh** having the parameters as at the point 2'. Due to the intensive mixing of liquid and vapor achieved in the vapor shell **Vsh** via the connecting pipes **CPs**, vapor and liquid of the stream 430 and 428 having the parameters as at the points 2'' and 2', respectively, are in equilibrium or very close to equilibrium, which is the purpose of the apparatus 400.

[0058] It must be noted that in all four cases set forth above, the liquid which is introduced into the apparatus is only a small portion of the total liquid available to the apparatus at any given time. Moreover, it is clear that, if needed, such an apparatuses can be installed consecutively (in series) and/or in parallel providing a process of effective vaporization of multi-component fluids having a wide range of boiling temperatures.

[0059] An apparatus based on the same principles, and designed for work at very high temperature (*e.g.*, in a direct coal fired power systems) is shown in **Figure 4**.

[0060] Referring now to **Figure 5**, a preferred embodiment of a very high temperature vaporization system of this invention, generally 500, is shown to include four heat transfer loops **HTL1-4**. The four heat transfer loops **HTL1-4** are designed to derive heat from an interior of a power plant furnace like a coal burning furnace. An input liquid stream 502, the stream to be vaporized, comprising saturated liquid and having parameters as at a point 51 is fed into the first heat transfer loop **HTL1** from a header **H**.

[0061] The stream 502, after being partially vaporized in the loop **HTL1**, becomes a first mixed stream 504 having parameters as at a point 52 and enters into a drum **D1**. In the drum **D1**, liquid is separated from vapor to form a first intermediate liquid stream 506 having parameters as at a point 53 and a first intermediate vapor stream 508 having parameters as at a point 61. The first intermediate liquid stream 508 having the parameters as at the point 53 passes through the second

heat transfer loop **HTL2**.

[0062] The stream **508**, after being partially vaporized in the loop **HTL2**, becomes a second mixed stream **510** having parameters as at a point **54** and enters a second drum **D2** along with the first intermediate vapor stream **508** having the parameters as at the point **61**. In the drum **D2**, liquid is separated from vapor to form a second intermediate liquid stream **512** having parameters as at a point **55** and a second intermediate vapor stream **514** having parameters as at a point **62**. The second intermediate liquid stream **512** having the parameters as at the point **55** passes through the third heat transfer loop **HTL3**.

[0063] The stream **512**, after being partially vaporized in the loop **HTL3**, becomes a third mixed stream **516** having parameters as at a point **56** and enters a third drum **D3** along with the second intermediate vapor stream **514** having the parameters as at the point **62**. In the drum **D3**, liquid is separated from vapor to form a third intermediate liquid stream **518** having parameters as at a point **57** and a second intermediate vapor stream **520** having parameters as at a point **63**. The third intermediate liquid stream **518** having the parameters as at the point **57** is combined with a fourth intermediate liquid stream **526** having parameters as at a point **59** as described below to form a combined stream **522** which then passes through the fourth heat transfer loop **HTL4**.

[0064] The stream **522**, after being partially vaporized in the loop **HTL4**, becomes a third mixed stream **524** having parameters as at a point **58** and enters a final drum **D4** along with the third intermediate vapor stream **520** having the parameters as at the point **63**. In the drum **D4**, liquid is separated from vapor to form the fourth intermediate liquid stream **526** having the parameters as at the point **59** and a final vapor stream **528** having parameters as at a point **64**. The fourth intermediate liquid stream **526** having the parameters as at the point **59** is combined with the third intermediate liquid stream **518** to form the combined stream **522** as described above.

[0065] It should be recognized by an ordinary artisan that the heat exchange process in each heat transfer loop **HTL1-4** are identical. Moreover, it should be recognized that four heat transfer loops is simply a convenient number for illustrating the process of this invention and the process can be operated by a minimum of 1 heat transfer loop and a maximum dependent on design criteria that can be as many as desired. Preferably, the number of heat transfer loops is between about 2 and about 20, particularly, between about 2 and about 16, and especially, between about 2 and 12.

[0066] As shown above, the proposed apparatus allows the maintenance of nucleate boiling in all heat transfer loops or heat exchangers where boiling occurs and at the same time, allows the production of vapor with the desired temperature and composition.

[0067] The apparatus provides for the full vaporization of multi-component fluids, the maintenance of high heat transfer coefficients in all boilers, and the protection of the boiler tubes from overheating in high temperature boilers.

[0068] In co-pending patent application bearing serial number (ref." 02019/05UTL), to achieve the same results, scrubbers were used in which the produced vapor would be brought into equilibrium with liquid by mixing in counter flow. The system proposed in the previous application also required that the process be performed in a minimum two heat exchangers. The use of scrubbers may require multiple introductions and removals of liquid and vapor into and from the scrubbers which requires a substantially complex control of the process.

[0069] This new apparatus does not require scrubbers. Effective equilibrium between vapor and liquid is achieved by multiple mixing of vapor and liquid, which occur essentially in the same apparatus as vaporization. Finally, the whole process of vaporization can be performed in just one apparatus if needed.

[0070] Referring now the **Figure 6**, a preferred a heat extraction and energy production facility of this invention, generally **600**, is shown to include a multi-component fluid vaporization apparatus of this invention **602**. The apparatus **602** includes a heat source input **604** and a heat source output **606**, where the input **604** inputs a heat source **608** shown here as an input heat source stream, but can be any other heat source and where the output **606** outputs a spent heat source **610** shown here as a spent heat source stream. Of course, if the heat source was focused sun light or other forms of electromagnetic radiation, then the input **604** would input light and the output **606** would output unused light.

[0071] The apparatus **602** also includes a liquid multi-component working fluid input **612** and a vapor multi-component working fluid output **614**, where the liquid input **612** inputs an input liquid multi-component working fluid stream **616** and where the vapor output **614** outputs a final vapor multi-component working fluid stream **618**. The final vapor stream **618** is input into an energy conversion unit **620** through a conversion unit vapor input **622**. Energy is extracted from the final vapor stream **618** to produce a spent stream **624**, which leaves the conversion unit **620** via a spent output **626**. The spent stream **624** is forwarded to a condensation unit **628** via a condensation input **630** and leaves the condensation unit **628** as the input liquid stream **616** via a condensation output **632**. Such energy conversion units can include any energy conversion unit known in the art including those described in United States Pat. Nos.: 4,346,561; 4,489,563; 4,548,043; 4,586,340; 4,604,867; 4,674,285; 4,732,005; 4,763,480; 4,899,545; 4,982,568; 5,029,444; 5,095,708; 5,440,882;

5,450,821; 5,572,871; 5,588,298; 5,603,218; 5,649,426; 5,754,613; 5,822,990; 5,950,433; 5,953,918; and 6,347,520; in co-pending United States Pat. Appln. Ser. Nos.: 10/242,301 filed 12 September 2002; 10/252,744 filed 23 September 2002; 10/320,345 filed 16 December 2002, and 10/357,328 filed 03 February 2003, 10/617367, filed 10 July 2003, and 10/ , filed 23 September 2003 bearing Express Mail Number EV 328 518 898 US, incorporated herein by reference.

[0072] Thus, the processes and apparatuses (systems) provide for the full vaporization of multi-component fluids, the maintenance of high heat transfer coefficients in the boilers, and the protection of the boiler tubes from overheating in high temperature boilers or other higher temperature heat transfer systems.

[0073] All references cited herein are incorporated herein by reference. While this invention has been described fully and completely, it should be understood that, within the scope of the appended claims, the invention may be practiced otherwise than as specifically described. Although the invention has been disclosed with reference to its preferred embodiments, from reading this description those of skill in the art may appreciate changes and modification that may be made which do not depart from the scope and spirit of the invention as described above and claimed hereafter.